

P6-7

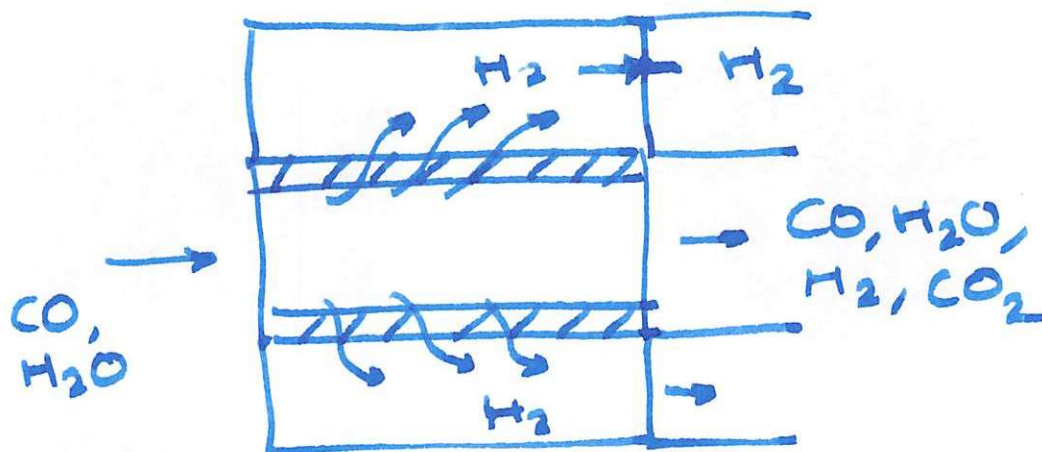
①

Fuel cell



Assumption

- Catalyst distributed evenly over whole volume



Mole balance

$$\frac{dF_A}{dW} = r'_A \quad \text{--- ①}$$

$$\frac{dF_B}{dW} = r'_B \quad \text{--- ②}$$

$$\frac{dF_C}{dW} = r'_C \quad \text{--- (3)}$$

$$\frac{dF_D}{dW} = r'_D - R_{H_2} \quad \text{--- (4)}$$

rate law:

$$r'_A = r'_B = -r'_C = -r'_D = r \quad \text{--- (5)}$$

$$r = -k \left[ C_A C_B - \frac{C_C C_D}{K_{eq}} \right] \quad \text{--- (6)}$$

$$R_{H_2} = K_{H_2} C_D \quad \text{--- (7)}$$

stoichiometry:

$$C_A = C_{T0} \frac{F_A}{F_T} ; C_B = C_{T0} \frac{F_B}{F_T} \quad \text{--- (8)}$$

$$C_D = C_{T0} \frac{F_D}{F_T} ; C_C = C_{T0} \frac{F_C}{F_T}$$

$$F_T = F_A + F_B + F_C + F_D \quad \text{--- (9)}$$

⇒ Solve eq<sup>n</sup>: ① - ⑨ numerically.  
to get answers to (a), (b), and (c)

(b) If membrane reactor is replaced by PFR, Hydrogen cannot escape.

⇒ maximum conversion that can be obtained is equilibrium conversion

$$K_{eq} = \frac{C_C C_D}{C_A C_B} = \frac{C_{A0}^2 x^2}{C_{A0}^2 (1-x)^2}$$

$$1.44 = \frac{x^2}{(1-x)^2} \Rightarrow x = 0.54$$

(c) If feed rate is doubled  $F_{A0}$ , and  $F_{B0}$  are doubled when solving ①-⑨