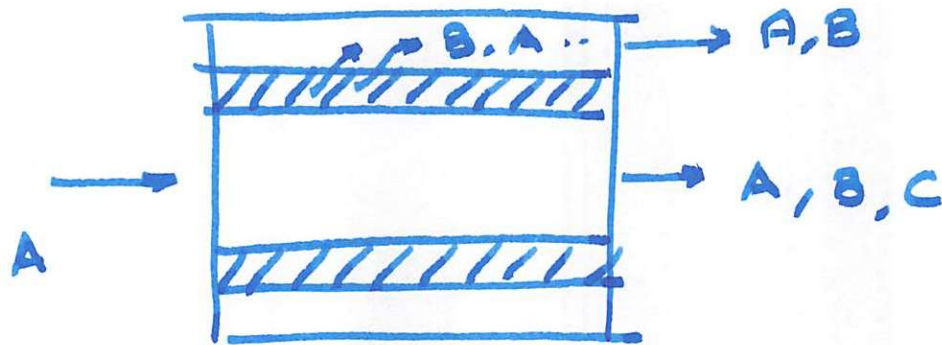


P-6-6

①

Membrane reactor



$$\begin{aligned} k &= 10 \text{ 1/min} & F_{A0} &= 100 \text{ mol/min} \\ K_C &= 0.01 \text{ mol/dm}^3 & J_0 &= 100 \text{ dm}^3/\text{min} \\ k_{CA} &= \cancel{1} \text{ 1/min} \quad 1 \text{ 1/min} & V &= 20 \text{ dm}^3 \\ k_{CB} &= 40 \text{ 1/min} \end{aligned}$$

A) Mole balance equations for A, B, and C need to be solved simultaneously.

$$\frac{dF_A}{dV} = r_A - R_A \quad \text{--- ①}$$

$$\frac{dF_B}{dV} = r_B - R_B \quad \text{--- ②}$$

} both A and B diffuse through membrane

$$\frac{dF_C}{dV} = r_C \quad \text{--- (3)}$$

$$-r_A = k \left[C_A - \frac{C_B C_C^2}{K_C} \right]$$

~~$$= k \left[\frac{C_{T0} F_A}{F_T} - \left(\frac{C_{T0} \right)^3 \left(\frac{F_B F_C^2}{K_C} \right) \right]$$~~

$$-r_A = k \left[\frac{C_{T0} F_A}{F_T} - \left(\frac{C_{T0} \right)^3 \left(\frac{F_B F_C^2}{K_C} \right) \right] \quad \text{--- (4)}$$

$$R_A = k_A C_A = \frac{k_{CA} C_{T0} F_A}{F_T} \quad \text{--- (5)}$$

$$R_B = k_{CB} C_B = \frac{k_{CB} C_{T0} F_B}{F_T} \quad \text{--- (6)}$$

Stoichiometry

$$-r_A = r_B = \frac{r_C}{2} \quad \text{--- (7)}$$

Solve eqⁿ: (1) - (7) numerically.

b) We need to solve eqⁿ: ~~8~~ - ~~9~~
simultaneously ~~8~~ - ~~10~~

$$\frac{dF_A}{dV} = r_A \quad \text{--- (8)}$$

$$\frac{dF_B}{dV} = r_B \quad \text{--- (9)}$$

$$\frac{dF_C}{dV} = r_C \quad \text{--- (10)}$$

c) conversion would be greater if C were diffusing out

→ rate of reverse reaction

$$-r_{rev} = k_r C_B C_C^2$$

2nd order w.r.t. C

P6-7

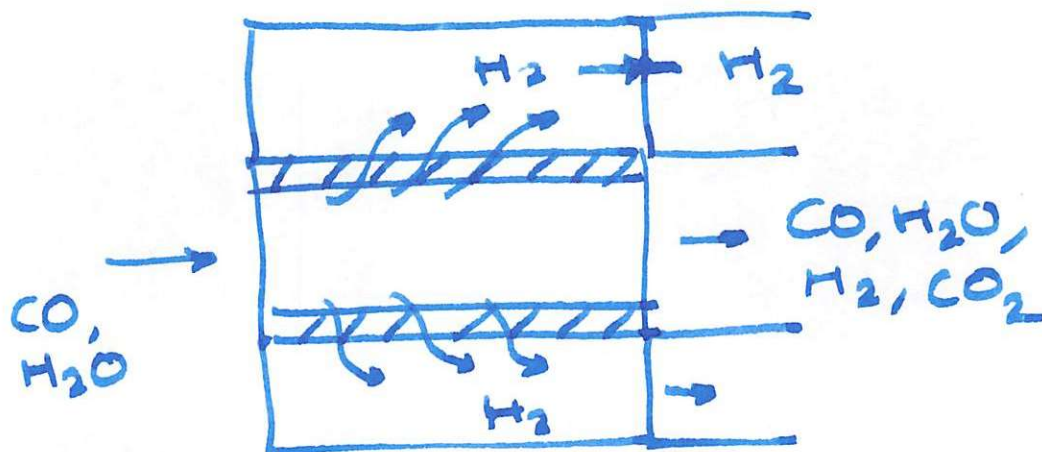
①

Fuel cell



Assumption

- Catalyst distributed evenly over whole volume



Mole balance

$$\frac{dF_A}{dW} = r'_A \quad \text{--- ①}$$

$$\frac{dF_B}{dW} = r'_B \quad \text{--- ②}$$