

Workshop 03: Rate law and stoichiometry

Lecture notes for chemical reaction engineering

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Try following problems from Fogler 5e (Fogler 2016).

P3-5, P3-10, P3-11, P3-12, P 4-6, P 4-8, P 4-11

We will go through some of these problems in the workshop.

P 3.12

Write the rate law for the following reactions assuming each reaction follows an elementary rate law. Give the units of k_A for each, keeping in mind some are homogeneous and some reactants are heterogeneous.

- $C_2H_6 \longrightarrow C_2H_4 + H_2$
- $C_2H_4 + \frac{1}{2} O_2 \longrightarrow C_2H_4O$
- $(CH_3)_3COOC(CH_3)_3 \rightleftharpoons C_2H_6 + 2 CH_3COCH_3$
- $nC_4H_{10} \rightleftharpoons iC_4H_{10}$
- $CH_3COOC_2H_5 + C_4H_9OH \rightleftharpoons CH_3COOC_4H_9 + C_2H_5OH$
- $2 CH_3NH_2 \xrightleftharpoons{cat} (CH_3)_2NH + NH_3$
- $(CH_3CO)_2O + H_2O \rightleftharpoons 2 CH_3COOH$

P3-10

The initial reaction rate for the elementary reaction $2 A + B \longrightarrow 4 C$ was measured as a function of temperature when the concentration of A was 2 M and that of B was 1.5 M.

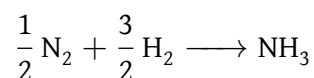
$-r_A$ (mol/dm ³ s)	T (K)
0.002	300
0.046	320
0.72	340
8.33	360

1. What is the activation energy?
2. What is the frequency factor?
3. What is the rate constant as a function of temperature using Equation 1 and $T_0 = 27^\circ\text{C}$ as the base case?

$$k(T) = k(T_0) \exp \left[\frac{E}{R} \left(\frac{1}{T_0} - \frac{1}{T} \right) \right] \quad (1)$$

P 4-8

The gas-phase reaction

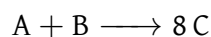


is to be carried out isothermally first in a flow reactor. The molar feed is 50% H_2 and 50% N_2 , at a pressure of 16.4 atm and at a temperature of 227°C .

- (a) Construct a complete stoichiometric table.
- (b) Express the concentrations in mol/dm^3 of each for the reacting species as a function of conversion. Evaluate C_{A0} , δ and ϵ , and then calculate the concentrations of ammonia and hydrogen when the conversion of H_2 is 60%.
- (c) Suppose by chance the reaction is elementary with $k_{\text{N}_2} = 40 \text{ dm}^3/\text{mol}/\text{s}$. Write the rate of reaction solely as a function of conversion for
 - (1) a flow reactor, and for
 - (2) a constant-volume batch reactor.

P 4-11

Consider a cylindrical batch reactor that has one end fitted with a frictionless piston attached to a spring (See Figure Figure 1). The reaction



with the rate law

$$-r_A = k_1 C_A^2 C_B$$

is taking place in this type of reactor.

- (a) Write the rate law solely as a function of conversion, numerically evaluating all possible symbols.
- (b) What is the conversion and rate of reaction when $V = 0.2 \text{ ft}^3$?

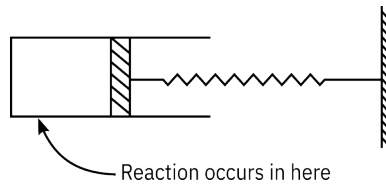


Figure 1: Cylindrical batch reactor

Additional information:

Equal moles of A and B are present at t_0

Initial volume: 0.15 ft^3

Value of k_1 : $1.0 (\text{ft}^3/\text{lbmol})^2 \cdot \text{s}^{-1}$

The spring constant is such that the relationship between the volume of the reactor and pressure within the reactor is

$$V = (0.1) (P) \text{ (V in } \text{ft}^3 \text{ , P in atm)}$$

Temperature of system (considered constant): 140°F

Gas constant: $0.73 \text{ ft}^3 \text{ atm}/\text{lbmol} \cdot ^\circ \text{R}$

Fogler, H. Scott. 2016. *Elements of Chemical Reaction Engineering*. Fifth edition. Boston: Prentice Hall.